The constant volume piezometer method is used to obtain $P, \rho, T$ data for propanol-l at temperatures of $150-370^{\circ} \mathrm{K}$ and pressures of $0.1-80 \mathrm{MPa}$.

The experimental data available in the literature on the $P, \rho, T$ properties of propanol-1 shows divergence in values by an amount greater than the sum of the experimental errors involved. Thus, although the results of [1] do agree basically with those of [2] within $0.5 \%$, nevertheless at low pressures and temperatures above $473^{\circ} \mathrm{K}$ the divergence between the respective data reaches several percent. The maximum deviation of data in [3] from those of [1] comprises $0.65 \%$ at $423^{\circ} \mathrm{K}$ and 50 MPa .

A study was made of $P, P, T$ behavior of $99.55 \%$ pure propanol-1 (density at $20^{\circ} \mathrm{C} 0.8046$ $\mathrm{g} / \mathrm{cm}^{3}$ ). The constant volume piezometer technique of [4] was used, with parasitic volumes eliminated by the use of a high-pressure valve operating at the experimental temperature. Data points were taken along both isobars and isotherms. The volume of the high-pressure vessel was measured at room temperature, and comprised $40.2020 \pm 0.0005 \mathrm{~cm}^{3}$. Thermal and baric corrections for the vessel were determined by the technique of [5] to an accuracy of 1 and $1.3 \%$, respectively. Total error in determination of vessel volume under experimental conditions was less than $0.013 \%$. The densities determined with consideration of all corrections had an uncertainty of less than $0.02 \%$, including reference error.

Pressure was measured by a class 0.05 piston manometer with two measurement columns at 600 and $2500 \mathrm{~kg} / \mathrm{cm}^{2}$, while temperature was determined with a platinum thermometer with error less than $0.01^{\circ} \mathrm{K}$.

Experimental results after coarse scale graphical processing for rounded pressure and temperature values are shown in Table 1.

At the conclusion of the $P, \rho, T$ experiments a pycnometer and type WA- 33 analytical scale were used to determine the normal densities of the propanol-1 studied and nine other samples of chemically pure grade propanol-1, produced in 1974-1978. The lowest density of $0.80352 \mathrm{~g} / \mathrm{cm}^{3}$ corresponded to a concentration of $99.95 \%$. This sample was diluted by distilled water to determine the dependence of density upon propanol content (Table 2).

Table 3 presents the liquid density on the saturation line for the $99.55 \%$ concentration,
TABLE 1. Density of Propanol-1 $\left(\mathrm{kg} / \mathrm{m}^{3}\right), \rho_{20}=0.8046$ ( $99.55 \%$ )

| T, ${ }^{\text {'K }}$ | $P$, MPa |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | 0,1 | 2.5 | 5 | 10 | 20 | 30 | 40 | 50 | 60 | 70 | 80 |
| 150 | 922,7 | 923,5 | 924,6 | 926,7 | 930,3 | 934.1 | 938,0 | 941,8 | 945, 4 | 948,7 | 951,6 |
| 170 | 903,5 | 904,8 | 905,9 | 908,1 | 912,5 | 916,4 | 920,7 | 924,6 | 928,4 | 931,7 | 934,8 |
| 190 | 886,5 | 887,6 | 888,8 | 891,1 | 895,9 | 900,3 | 904,8 | 909,0 | 913,1 | 916,7 | 919,9 |
| 210 | 870,6 | 871,7 | 873, 1 | 875,4 | 880,2 | 885,1 | 889,9 | 894,4 | 898,4 | 902,2 | 905,6 |
| 230 | 854,4 | 855,7 | 857,2 | 859,8 | 864,9 | 870.1 | 875,2 | 879,9 | 884,4 | 888,5 | 892,2 |
| 250 | 838,5 | 839,8 | 841,4 | 844,1 | \$49,8 | 855,4 | 860,8 | 865.9 | 870,5 | 875,2 | 879,2 |
| 270 | 823,0 | 824, 5 | 826,1 | 829,1 | 835,3 | 841,6 | 847,4 | 852,8 | 857,5 | 862,1 | 866,4 |
| 290 | 807,2 | 809,2 | 811,3 | 814,8 | 821,8 | 828,2 | 834,1 | 839,7 | 845,2 | 849,9 | 854,4 |
| 310 | 791,4 | 794,0 | 796,3 | 799,9 | 807,5 | 814,4 | 820,9 | 826,8 | 832,4 | 837,6 | 842,6 |
| 330 | 774,8 | 777,4 | 780,1 | 784,4 | 792,7 | 800, 1 | 807,1 | 813,4 | 819,2 | 824,7 | 830, 1 |
| 350 | 757,6 | 760,2 | 763,2 | 768,4 | 777,6 | 785,4 | 792,5 | 799,4 | 805,7 | 811,8 | 817,5 |
| 370 | 739,6 | 742,7 | 745,3 | 751,6 | 761,8 | 770,3 | 778,1 | 785,1 | 791,7 | 797,7 | 803,3 |

Physics Institute, Dagestan Branch, Academy of Sciences of the USSR, Makhachkala. Translated from Inzhenerno-Fizicheskii Zhurnal, Vol. 43, No. 5, pp. 796-798, November, 1982. Original article submitted August 21, 1981.

TABLE 2. Density vs Propanol-1 Concentration at $20.0^{\circ} \mathrm{C}$

| $K, \%$ | 70,654 | 80,093 | 89,771 | 96,333 | 99,500 | 99,550 | 99,95 | 100,00 |
| :--- | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\rho, \mathrm{~kg} / \mathrm{m}^{3}$ | 853,37 | 841,45 | 826,37 | 812,40 | 804,80 | 804,60 | 803,52 | $803,48^{*}$ |

*Extrapolation.
TABLE 3. Liquid Propanol-1 Density on Saturation Line (99.55\%)

| $\tau, \mathrm{K}$ | $\rho, \mathrm{kg} / \mathrm{m}^{3}$ | $\tau, \mathrm{~K}$ | $\rho, \mathrm{~kg} / \mathrm{m}^{3}$ |
| :---: | :---: | :---: | :---: |
| 150 | 922,7 |  | 270 |
| 170 | 903,6 | 290 | 822,8 |
| 190 | 886,6 | 310 | 807,3 |
| 210 | 870,1 | 330 | 791,1 |
| 230 | 854,1 | 350 | 774,3 |
| 250 | 838,6 | 370 | 756,4 |
|  |  |  | 736,6 |

determined both from the $P, \rho, T$ experiment, and by finding the temperature of transition from the two-phase state to a single phase with slow heating of the specimen.

The results obtained were compared with those of [1]. Table 2 was used to determine the density of the specimen used in [1], which proved equal to $0.8037 \mathrm{~g} / \mathrm{cm}^{3}$ at $20^{\circ} \mathrm{C}$. The specimen density in the present experiments was $0.0009 \mathrm{~g} / \mathrm{cm}^{3}$ higher. With consideration of this difference, the agreement at the $350^{\circ} \mathrm{K}$ isotherm lies within the limits of experimental uncertainity of [1], i.e., $0.1 \%$. At the same time, at the $200^{\circ} \mathrm{K}$ isotherm there is a divergence exceeding the net uncertainty of the experiments. The divergence decreases from 0.35 to $0.15 \%$ with increase in pressure from 2.0 to 50.0 MPa . The data of [1] are elevated compared to those of the present study. Apparently, this divergence can be explained by experimental peculiarities of the technique used in [1] and the significant increase in specimen viscosity with reduction in temperature, which makes achievement of an equilibrium position by the float difficult.

## NOTATION

P, pressure, $\mathrm{MPa} ; \rho$, density, $\mathrm{kg} / \mathrm{m}^{3} ; \mathrm{T}$, temperature, ${ }^{\circ} \mathrm{K}$.

## LITERATURE CITED

1. I. F. Golubev, T. N. Vasil'kovskaya, and V. S. Zolin, "Experimental study of aliphatic alcohol densities at various temperatures and pressures," Inzh.-Fiz. Zh., 38, No. 4, 688-670 (1980).
2. I. F. Golubev and E. N. Vagina, "Specific gravity of n-propyl, isopropyl, n-butyl, and isobutyl alcohols at high pressure and various temperatures," $\operatorname{Tr}$. GIAP, 15, 39-55 (1963).
3. E. I. Konikevich, "Study of the thermal properties of liquid aliphatic alcohols and their solutions," Author's Abstract of Candidate's Dissertation, Moscow (1977).
4. Z. R. Zakar'yaev, "Universal thermophysical apparatus for P, $\rho, \mathrm{T}, \mathrm{C}_{\mathrm{V}}$-experiments with liquids," in: Thermophysical Properties of Liquids and Gases [in Russian], Dagestan Branch, Academy of Sciences of the USSR, Inst. Fiz., Makhachkala (1979), pp. 52-63.
5. Z. R. Zakar'yaev, "Thermal and baric deformations of high pressure vessels," Dep. VINITI, No. 11(97), 87 (1979).
